

# Catalytic Effect of $\text{TiF}_3$ on Hydrogenation Properties of $\text{MgH}_2$

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**Abstract-** Magnesium based hydrides are attractive materials for hydrogen storage with reversible hydrogen capacity up to 7.6 wt%. However, the potential for commercial applications of  $\text{MgH}_2$  is limited because of its high temperature of hydrogen discharge and slow desorption kinetics.

The present work deals with investigating the catalytic effect of  $\text{TiF}_3$  on hydrogenation properties of  $\text{MgH}_2$ . The samples are prepared by ball milling  $\text{MgH}_2$  with varying concentration of  $\text{TiF}_3$  at different milling time. Absorption/desorption kinetics were studied by Sievert's type apparatus under different temperatures. The subsequent changes in structural and morphological properties induced by hydrogenation / dehydrogenation are studied using XRD and SEM. Results indicate that the catalyst enhances the kinetics of pure  $\text{MgH}_2$  with stability in capacity.  $\text{MgH}_2$ +10wt%  $\text{TiF}_3$  ball milled for two hour was found to absorb 3wt% hydrogen at 573K temperature.

**Keywords-** Hydrogen Storage, transition metal fluoride, Ball milling, catalyst, kinetics.

## I. INTRODUCTION

Due to high gravimetric (7.6%) and volumetric (110  $\text{kgm}^{-3}$ ) hydrogen capacity, low cost, high abundance and good reversibility  $\text{MgH}_2$  has been considered as a one of the most promising material for hydrogen storage. However its practical onboard application for hydrogen storage is impeded by its high operating temperature and sluggish hydriding/dehydriding kinetics [1]. Various studies have been carried out to enhance the hydrogen sorption properties of nano crystalline  $\text{MgH}_2$  by adding suitable catalysts such as transition metal, their oxides and halides. Among various additives  $\text{Nb}_2\text{O}_5$  possesses an impressive catalytic effect on the sorption kinetics of  $\text{MgH}_2$  [2].

Recently it has been reported that metal halide catalyst addition results in better hydrogen storage than their metal or metal oxides. Bhat *et al.* [3] compared the effect of  $\text{Nb}_2\text{O}_5$  with its halide  $\text{NbCl}_5$ . They found that  $\text{NbCl}_5$  shows better catalytic effect than  $\text{Nb}_2\text{O}_5$ . The influence of niobium oxide and halide on the hydrogen desorption properties of ball milled  $\text{MgH}_2$  have been investigated by Recham *et al* [4] and found that the halides show faster kinetics and reduced hydrogen desorption temperature. It has also been found that some transition metal halides, such as  $\text{CrCl}_3$ ,  $\text{FeF}_3$ ,  $\text{NiF}_2$ ,  $\text{TiF}_3$ ,  $\text{NbCl}_5$  and  $\text{NbF}_5$ , also show very good catalytic property [5- 12]. Jin *et al.*[13] investigated the effect of various halide additives ( $\text{NiF}_2$ ,  $\text{TiF}_3$ ,  $\text{VF}_4$ ,  $\text{NbF}_5$ ,  $\text{FeF}_2$ ,  $\text{ZrF}_4$ ,  $\text{CrF}_2$ ,  $\text{CuF}_2$ ,  $\text{CeF}_3$ ,  $\text{YF}_3$ ) on the decomposition temperature of  $\text{MgH}_2$  by DSC method and found that Ni, Ti, V and Nb fluorides are more effective than Fe, Zr, and Cr, while  $\text{CuF}_2$ ,  $\text{YF}_3$  and  $\text{CeF}_3$  do not have a significant catalytic effect.

Malka *et al.* [14] studied the influence of various halide additives (chlorides and fluorides) on the decomposition temperature of  $\text{MgH}_2$  using the TPD method and reported that fluorides are better catalyst than chlorides. Halides having highest oxidation state reduce magnesium decomposition temperature more effectively than their counterparts with lower oxidation state. Halide from group IV and V of the periodic table are better catalysts in comparison to the other studied halide [14]. During the ball milling  $\text{MgH}_2$  react with fluorides and formed a protective and reactive layer of  $\text{MgF}_2$ . This compound has a high affinity with hydrogen because of the F-anion, which weakens the Mg-H bonding and improves the sorption properties [15- 17].

In this paper influence of  $\text{TiF}_3$  halide (with various concentrations) additive on the hydrogenation

properties of ball milled  $\text{MgH}_2$  at different milling time has investigated. This system possesses enhanced sorption kinetics, in particular the absorption performance at a moderate temperature range.

## II. EXPERIMENTAL

Pure  $\text{MgH}_2$  (purity 98%) and  $\text{TiF}_3$ (98%)were purchased from Alfa Aesar. Ball milling was carried out, nominally at Room Temperature (RT) using planetary (Retsch PM 100 type) ball mill. The vial and ball materials were hardened chromium steel. To start with  $\text{MgH}_2$  was milled in Argon (Ar) atmosphere for 20 hours at RT. Then  $\text{MgH}_2 + x$  wt%  $\text{TiF}_3$  ( $x = 5, 10 \& 15$ ) were ball milled for 2 and 5 h under Ar atmospheric condition. The powder specimen was loaded into the vial then sealed using an O-ring covered with a thin layer of sealing grease in an Ar filled homemade Glove box at our laboratory in University of Rajasthan Jaipur, India. The ball-to-powder mass-charge ratio (BPR) was approximately 40:1 and the milling speed has been maintained at 300 rpm for different milling periods.

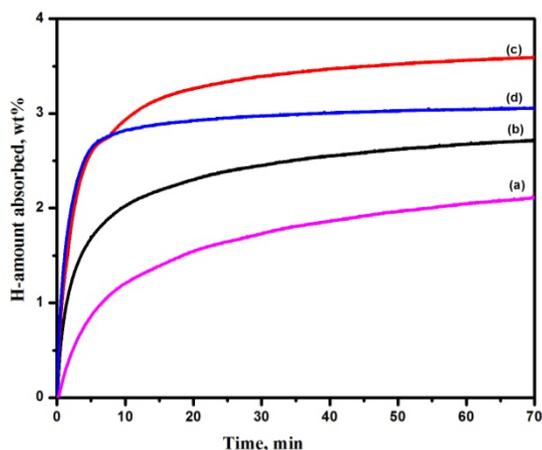


Fig.1. Hydrogen absorption curves at 573 K of (a) 20 hrs milled  $\text{MgH}_2$ , (b)-(d) 2 hrs milled  $\text{MgH}_2 + x$ wt%  $\text{TiF}_3$  ( $x = 5, 10, 15$ ).

Hydrogenation storage properties of  $\text{TiF}_3$  doped  $\text{MgH}_2$  were investigated at different temperatures by using a Sievert-type apparatus which was built up in our lab. Prior to study the whole system was evacuated to  $10^{-6}$  Torr vacuum at 673 K for 2 h and the samples were introduced for hydrogenation in the chamber. To perform hydrogenation measurement one gram of the

as-milled sample was kept in a stainless steel cylindrical vial (5 ml capacity) and closed with a filtered stainless steel cap and inserted in the stainless steel high pressure reactor (20 ml capacity). Before measurements sample was completely desorbed at 350  $^{\circ}\text{C}$  under vacuum of  $1 \times 10^{-6}$  Torr.

The structures of the samples were characterized by X-ray Diffraction (XRD, Panalytical Make X' Pert PRO MPD) analysis using  $\text{CuK}\alpha$  radiation ( $\lambda = 1.54 \text{ \AA}$ ). Particle size and surface topology of all the samples were investigated using Scanning Electron Microscope (SEM, ZEISS with EHT 20.00 Kv).

## III. RESULTS AND DISCUSSION

### A. Effect of the addition of $\text{TiF}_3$

The hydrogen sorption kinetics of  $\text{MgH}_2$ , by mechanical milling with additives can be markedly improved at near room temperature. The catalytically enhanced kinetic performance was found to persist in the absorption/desorption cycles. But the catalytic mechanism has not yet been well established. The absorption curves of 20 and 2 hrs milled  $\text{MgH}_2$  and  $\text{MgH}_2 + x$  wt%  $\text{TiF}_3$  ( $x = 5, 10, 15$ ) are shown in Fig. 1 respectively.

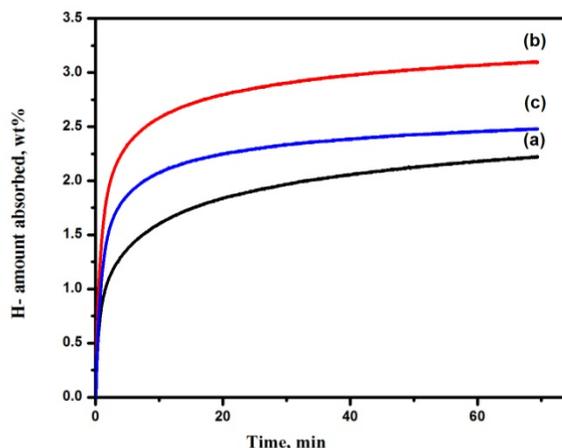


Fig.2. Hydrogen absorption curves at 523 K of 2 h milled  $\text{MgH}_2 + x$  wt%  $\text{TiF}_3$ (a)-(c) for 5, 10 and 15wt%.

It is observed that the addition of different amount of Catalyst improved the absorption kinetics of  $\text{MgH}_2$ . From 5- 10 wt% of  $\text{TiF}_3$  hydrogen absorption capacity increased as well as absorption kinetics but further with increasing concentration of catalyst hydrogen capacity

decreased. The absorbed amount of hydrogen are 2, 3 and 2.8 wt% for  $\text{MgH}_2+x$  wt%  $\text{TiF}_3$  ( $x = 5, 10, \text{ and } 15$ ) in first 10 minutes. Here we report additional results at lower operating temperature (523 K) and found that the absorbed amount of hydrogen is decreased to about 1.5, 2.5 and 2.0 wt% for the additives concentration ( $x = 5 - 15$ ) of  $\text{TiF}_3$  as shown in Fig.2. It is concluded that the highest storage capacity is 3 wt% for the  $\text{MgH}_2$ -10 wt%  $\text{TiF}_3$ . The results also show that the high concentration of  $\text{TiF}_3$  catalyst will degrade the hydrogen storage capacity of the material, as seen from the profile of the sample containing 15 wt%  $\text{TiF}_3$ .

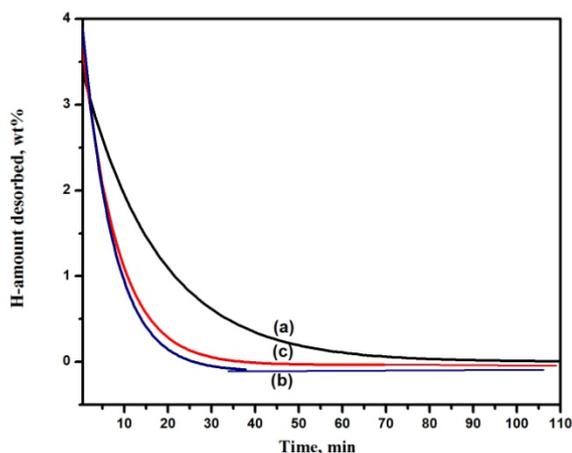


Fig. 3. Hydrogen desorption curves at 573 K of  $\text{MgH}_2+x$  wt%  $\text{TiF}_3$  for  $x = 5, 10, 15$  in (a), (b) and (c).

Therefore, 2 h milled  $\text{MgH}_2+10$  wt%  $\text{TiF}_3$  is selected for further investigation of structural properties of as-milled and hydrogenated/ de-hydrogenated samples and hydrogen storage capacity at different operating temperatures (below  $300^\circ\text{C}$ ).

The pronounced catalytic enhancement arising upon adding of  $\text{TiF}_3$  was also observed on the hydrogen desorption properties. Fig. 3 shows the desorption curves at 573 K of 2 h milled  $\text{MgH}_2+ x$  wt%  $\text{TiF}_3$  ( $x = 5, 10, 15$ ). It is clear from the desorption results, that more hydrogen is released in the same time limit from the 10 wt%  $\text{TiF}_3$  than the other ones. Addition of  $\text{TiF}_3$  improved the desorption kinetics of  $\text{MgH}_2$  by accelerated desorption rate and reduced operating temperature.

### B. Effect of milling time

The effect of milling time on  $\text{MgH}_2+10$  wt%  $\text{TiF}_3$  for 2 and 5 hrs are shown in Fig. 4. Apparently, a longer milling time leads to a more pronounced kinetic enhancement in particular during the initial periods.

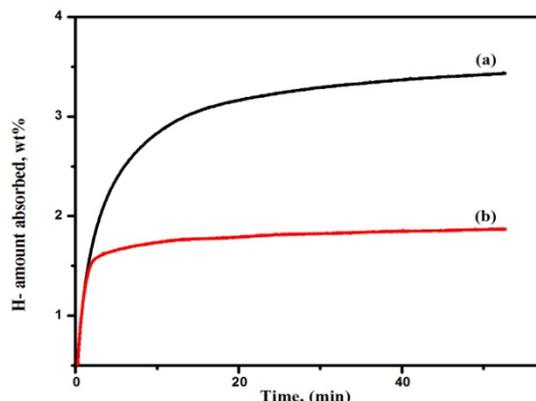


Fig.4. Comparison of hydrogen absorption of ball milled  $\text{MgH}_2+10$  wt%  $\text{TiF}_3$  at 573 K for (a) 2 h (b) 5 h.

However, it is also observed that increasing milling time causes a substantial decrease in the hydrogen capacity. Hydrogen storage of  $\text{MgH}_2+10$  wt%  $\text{TiF}_3$  at 573 K is observed to be 3.0 wt% in 10 minutes for 2 hrs milled while for 5 hrs milled it's decreased to  $\sim 1.7$  wt%.

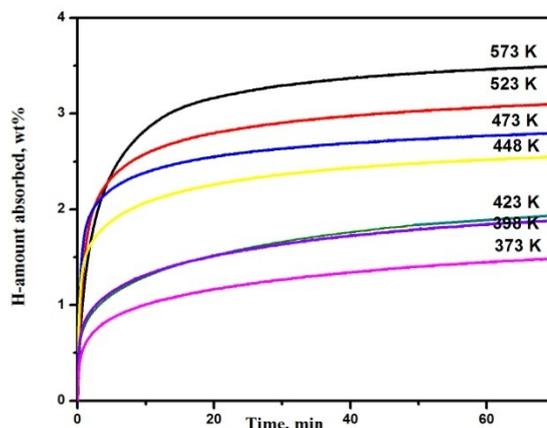


Fig. 5. Hydrogen absorption curves of  $\text{MgH}_2+10$  wt%  $\text{TiF}_3$  at temperature range from 573 K to 373 K in the curves of (a) – (g) respectively

### C. Hydrogen storage performance

Hydrogen storage performance of 2 hour milled  $\text{MgH}_2$ +xwt%  $\text{TiF}_3$  was further investigated for the temperature range from 573 K to 373 K which are shown in fig. 5 from (a)-(g). Generally pre-activation is required for the pure  $\text{MgH}_2$  however, in case of  $\text{MgH}_2$  catalyzed with  $\text{TiF}_3$  or any other transition metal halides pre-activation is not required and sample is directly used for the measurements after complete desorption at 573 K for 2 h. In case of 2 h milled  $\text{MgH}_2$ +10 wt%  $\text{TiF}_3$  the absorbed hydrogen amount was found 3 wt% within 10 minutes and was about to saturate in one hr for the temperature range 523–448 K. The hydrogen capacity of this material is decreased by half of the above capacity in the temperature range from 423 – 373 K. It is concluded from the results that the increment in hydrogen storage capacity is due to the catalytic effect of  $\text{TiF}_3$  on  $\text{MgH}_2$  in the starting time periods (~10 minutes).

### D. Structural characterization

The catalytic effect of 10 wt%  $\text{TiF}_3$  on structural properties of  $\text{MgH}_2$  have been investigated using X-ray diffraction (XRD) and scanning electron microscopy (SEM). Fig.6 shows the diffraction patterns of 2 h milled  $\text{MgH}_2$ +10wt%  $\text{TiF}_3$  for as-prepared, hydrogenated and dehydrogenated samples. It is clear from the results that diffraction pattern of as-milled sample is quite similar to  $\text{MgH}_2$ . The qualitative result obtained from weak and broad peaks shows that the grain size decreases and lattice strain increases [18].

In the case of the as-milled sample, the most intense Bragg peaks are identified as tetragonal  $\beta$ - $\text{MgH}_2$  and a metastable orthorhombic phase  $\gamma$ - $\text{MgH}_2$  which has been previously reported to form upon milling  $\text{MgH}_2$  [19]. It is observed from the diffraction patterns that the intensity of  $\beta$ - $\text{MgH}_2$  peak increased after hydrogenation and disappeared after dehydrogenation. Besides, the formation of a  $\gamma$ -  $\text{MgH}_2$  induced by high energy milling is also observed and disappears in the dehydrogenation process as in case of  $\beta$ - $\text{MgH}_2$  peak.

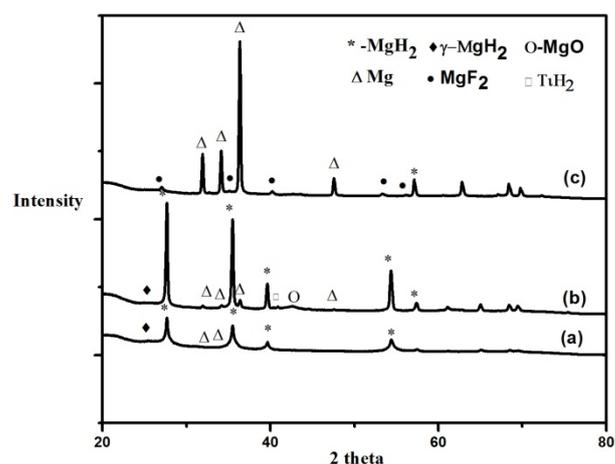


Fig.6. XRD patterns of the  $\text{MgH}_2$ +10wt%  $\text{TiF}_3$  (a) as prepared, (b) hydrogenated and (c) after desorption.

In the present case  $\text{MgO}$  was detected in both samples except dehydrogenated sample, which is likely due to the slight oxygen contamination. No peak related to  $\text{TiF}_3$  is identified in as-milled sample. After dehydrogenation process  $\text{MgF}_2$  and  $\text{TiH}_2$  peak were observed, suggesting that  $\text{MgH}_2$  reacts with  $\text{TiF}_3$  to produce  $\text{MgF}_2$ . When  $\text{MgH}_2$  reacts with fluorides,  $\text{MgF}_2$  is usually formed as a protective and reactive layer during the reaction between  $\text{MgH}_2$  and titanium or metal fluoride [3, 4, 6, 20]. This compound possesses a high affinity with hydrogen because of the F- anion, which weakens the Mg-H bonding and improves the sorption properties [4]. The formation of these two phases should follow reaction (1). It is highly expected that this reaction can occur during milling process due to collision between vial, balls and among the balls produced high energy environment.

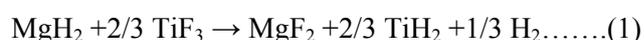


Fig.7 shows the SEM micrographs of 2 h milled  $\text{MgH}_2$ +10%wt  $\text{TiF}_3$  and subsequently hydrogenated-dehydrogenate at 573 K. The results indicate that the particle size of  $\text{MgH}_2$  is effectively decreased after ball milling and found many particles distribution at the surface of the composite matrix. The decrease of

particle size can enhance the rates of hydrogenation-dehydrogenation.

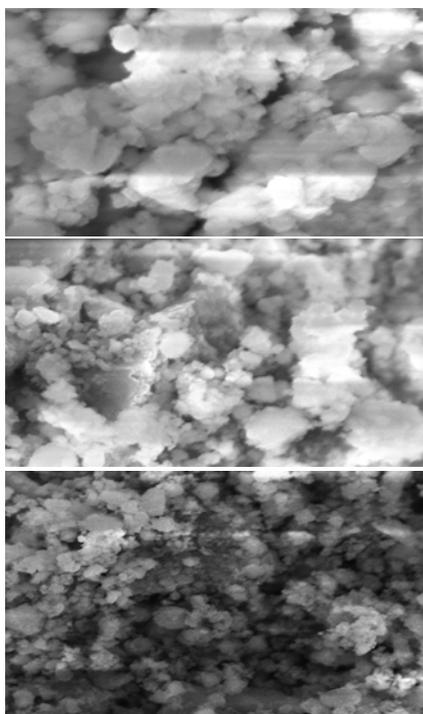


Fig.7. SEM images of 2h milled  $\text{MgH}_2+10 \text{ wt}\% \text{ TiF}_3$  (a) as milled (b) hydrogenated and (c) dehydrogenation.

#### IV. CONCLUSIONS

Titanium fluorides that readily react with  $\text{MgH}_2$  to form hydrides or metal–hydrogen solid solutions tend to exert a significant catalytic effect on the hydrogenation kinetics of  $\text{MgH}_2$ .

It is concluded that the various concentration of catalyst ( $\text{TiF}_3$ ) improved the absorption/ desorption kinetics of  $\text{MgH}_2$ . The 2 h milled  $\text{MgH}_2+10 \text{ wt}\% \text{ TiF}_3$  absorbed hydrogen 3 wt% within 10 minutes and about to saturate in one hr at below operating temperature while the hydrogen desorption was the same wt% in time limit. The storage capacity of  $\text{MgH}_2+10 \text{ wt}\% \text{ TiF}_3$  at operating temperature 573 K is decreased with increasing milling time and decreased by  $\sim 1.7 \text{ wt}\%$  in 10 minutes.

The microstructure and XRD analysis show that  $\text{MgF}_2$  and  $\text{TiH}_2$  phases form in the dehydrogenation process for the 2 h milled  $\text{MgH}_2-10 \text{ wt}\% \text{ TiF}_3$  sample.

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